

Project Initiation: First Steps

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Waste Heat/Recovered Energy

- Primarily in the form of:
 - Combustion gases
 - Hot air
 - Hot water
- Sometimes:
 - Low pressure steam
 - Non-steam vapors (hydrocarbons)



Prerequisites

- Ample supply of waste heat
 - >200F liquid, >400F gas
 - Clean
 - Accessible
- High cost power (>\$.08/kWh)
 - PPA for excess not used internally
- Continuous process (>7000 hr/yr)
- No need for additional process heat
- Upsets tolerated



Goal

□ Financial return

- Project all-in cost of generation < internal

- $C_T = C_{CR} + \cancel{\text{Fuel}} + C_{OPEX}$

- No fuel, capital recovery dominates
- Efficiency is less important than energy utilization
- Efficiency only matters to the extent that it reduces \$/kW

□ Reduce emissions

- Environmental steward, “green” is good

□ Energy security

- Grid independence
- Less susceptible to higher rates



Total Generation Cost

□ All-in cost of generation

■ $C_T = C_{CR} + \cancel{\text{Fuel}} + C_{OPEX}$

□ $C_{CR} = \text{Capital Recovery} = (C_{RF} \times \$/\text{kW})/\text{UTIL}$

□ $C_{RF} = \text{Recovery Factor; } 10\% \text{ +/- for debt; } 20\% \text{ +/- for equity}$

□ Example

■ $C_{RF} = 16\%$, CAPEX = \$2000/kW, UTIL = 8000 h/yr,
OPEX = \$.01/kWh

■ $C_T = (.16 \times 2000)/8000 + .01$
 $= \$.05/\text{kWh}$



Feasibility Criteria

- Project Output ~kW
 - Characterize waste heat
 - Quantity and quality
- Cost
 - CAPEX and OPEX
- Utilization
 - Baseload vs. intermittent
- Risk
 - Source temperature too high?
 - Corrosion/deposition/erosion
 - Interface w/must run process



Project Output

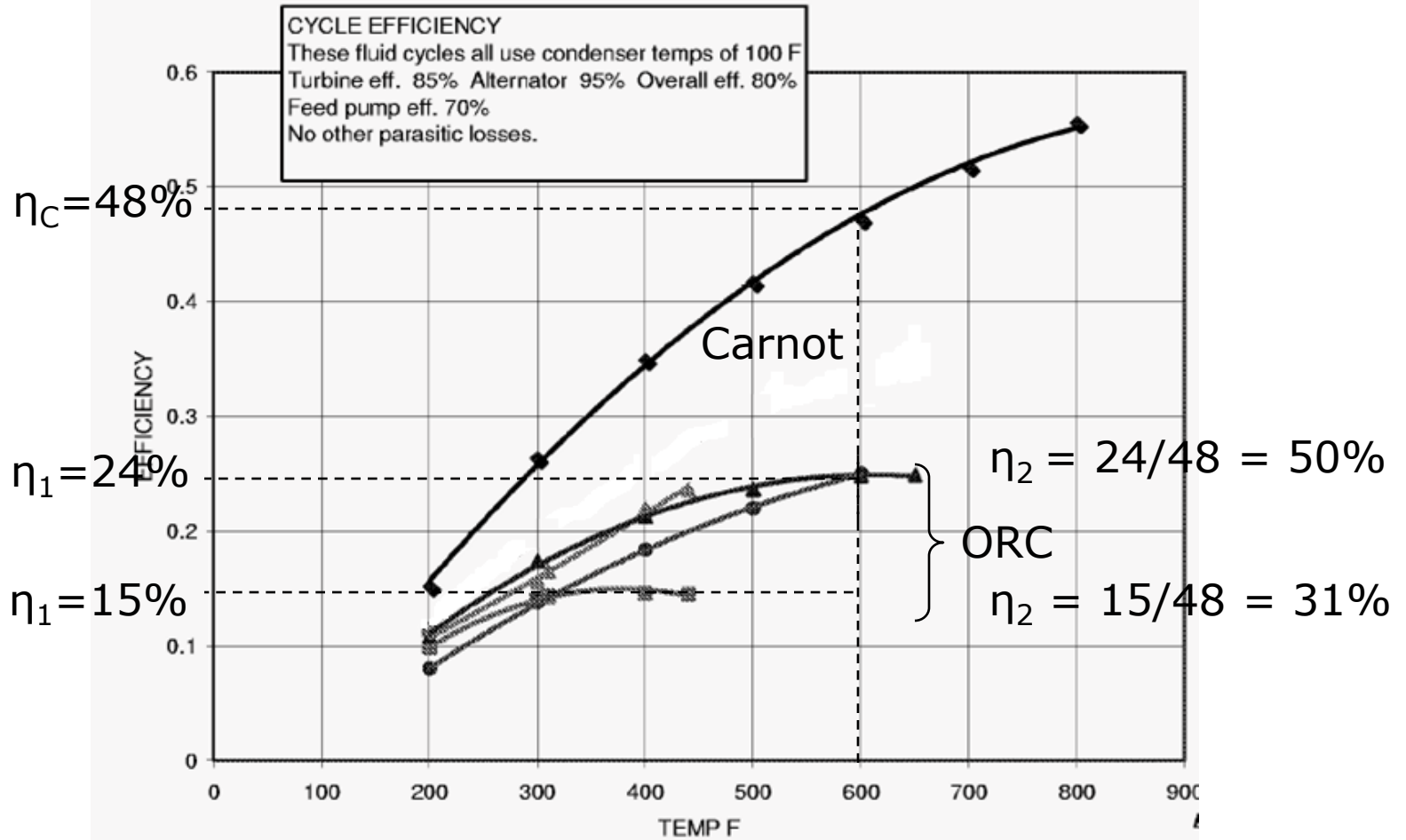
- Output (W) = Energy (ΔH) $\times \eta_1$
 - Energy content (Btu/h or kW thermal) is *quantitative*
 - First Law
 - $\Delta H = m \times c_p \times (T_1 - T_2)$
 - T_1 = initial source temp, T_2 = final source temp
 - Need to find plant (thermal) efficiency, η_1

- Determine *quality* of waste heat to find η_1
 - Exergy content
 - Second Law: $E = \Delta H \times [1 - T_0(\ln T_1/T_2)/(T_1 - T_2)]$
 - Assumes T_0 (cooling water) = constant



Cycle Efficiency

ORC vs. Carnot



Source: Barber Nichols



Output Estimate

Theoretical (Carnot) eff'y:

$$\eta_c = [1 - T_0(\ln T_1/T_2)/(T_1 - T_2)]$$

Internal eff'y (Second Law):

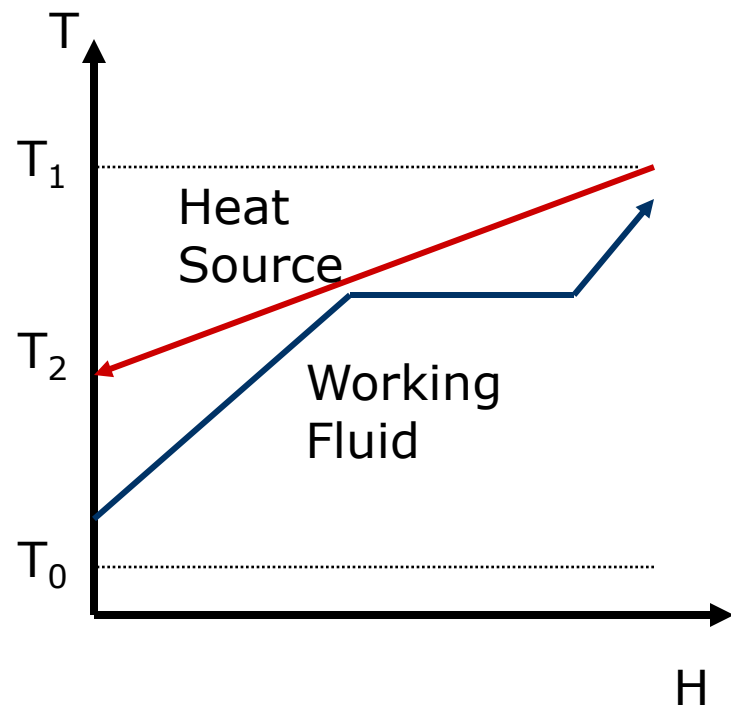
$$\eta_2 = \eta_1 / \eta_c ; 30\% < \eta_2 < 50\%$$

Thermal (First Law) eff'y:

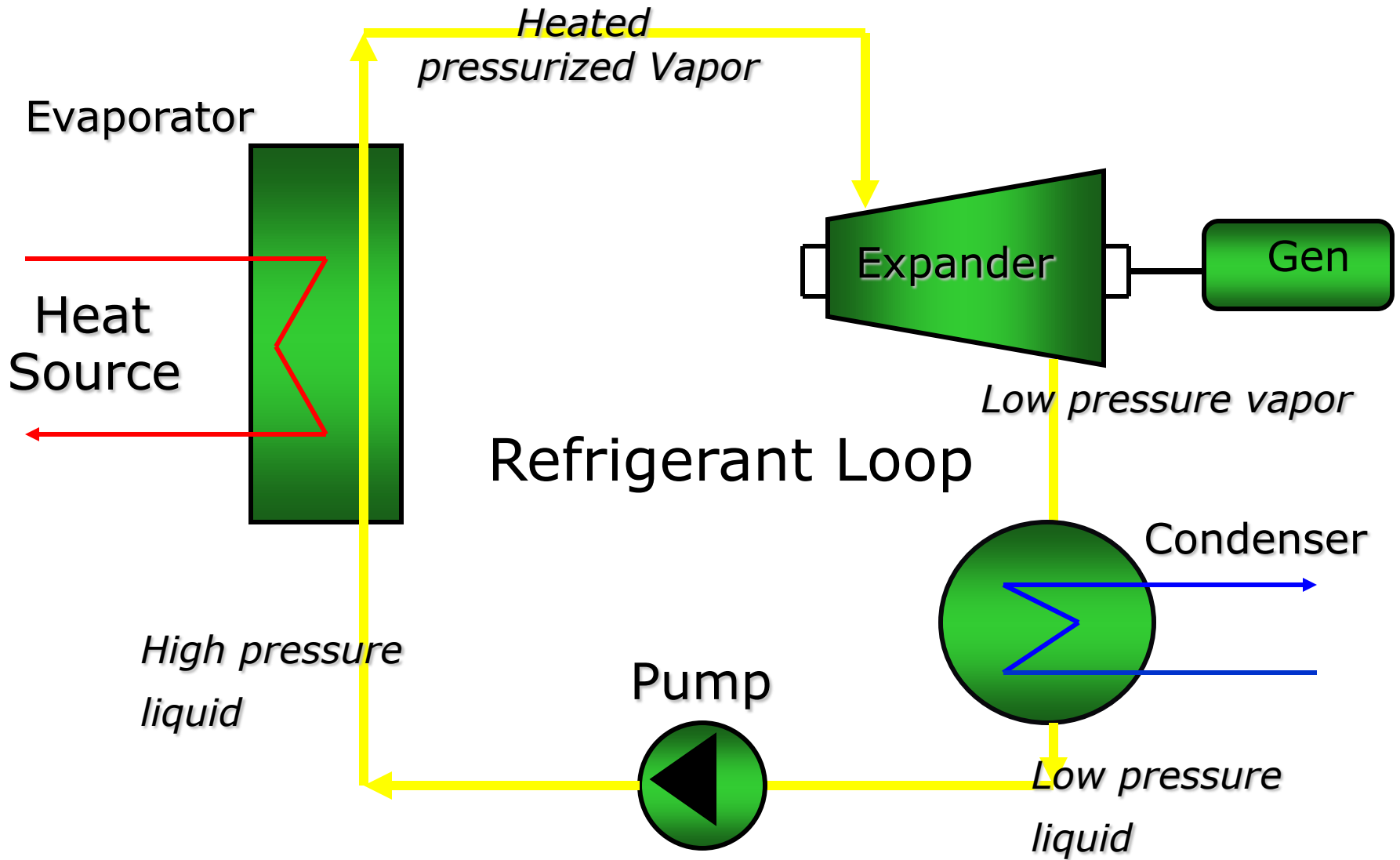
$$\eta_1 = \eta_2 / \eta_c$$

$$W = \Delta H \times \eta_1$$

Heat Acquisition Process

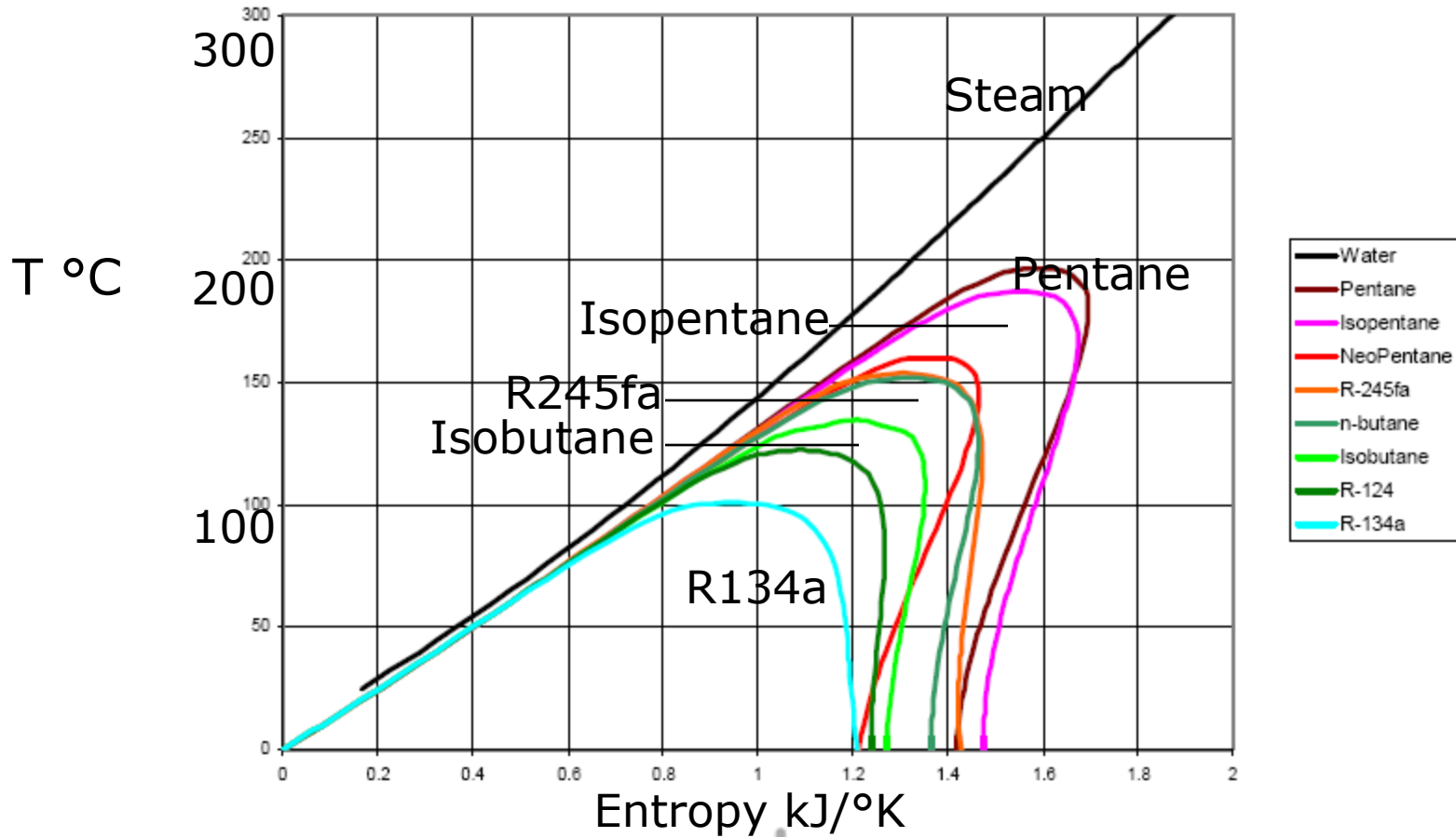


Organic Rankine Cycle



Working Fluid Selection

T-s diagram



Cycle and Fluid Selection

- Cycles
 - ORC
 - Ammonia Water (Kalina, Absorption)
- Working Fluids (Refrigerants)
 - Performance (Cycle output)
 - Cost
 - Stability at elevated temperature
 - Safety
 - Reliability
 - Vacuum
 - Operator requirements



Steam vs. ORC

Steam

- >700F
- >10 MW
- $\eta_1 = 20-30\%$
- Water available
- Licensed operators
- Complex
 - Vacuum
 - Condensate polish
 - Blow down

ORC

- <700F
- <10 MW
- $\eta_1 = 10-20\%$
- No water
- Little or no supervision
- Closed system
 - Above atmospheric
 - No fluid treatment
 - No blow down



Equipment

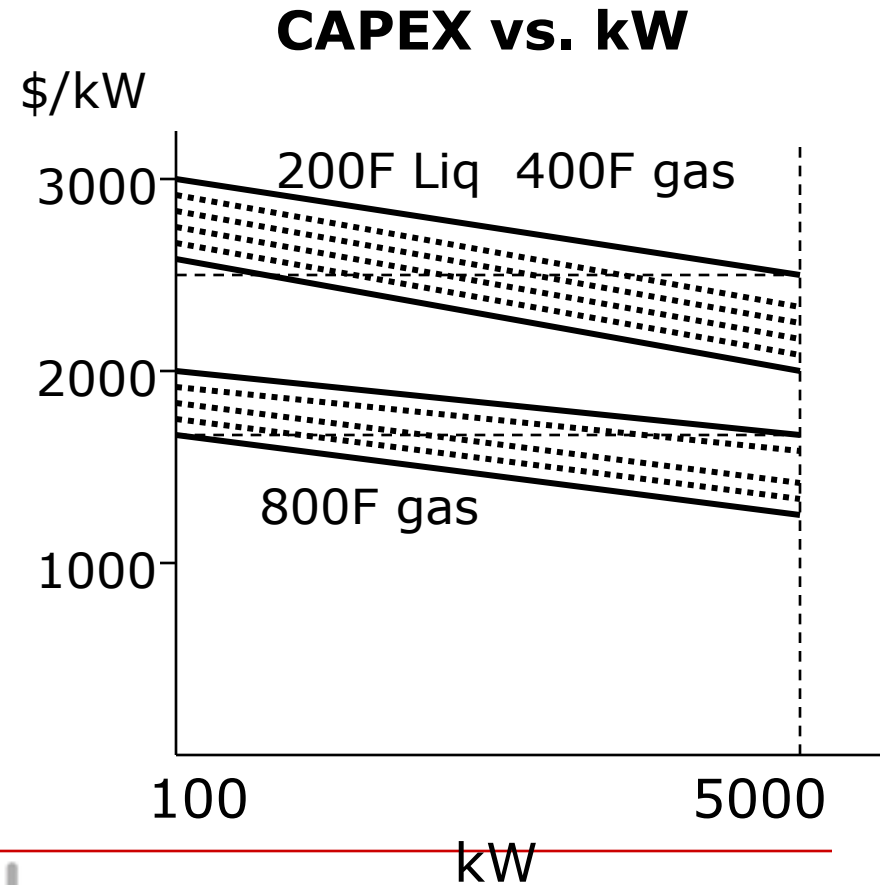
- Expander/Generator
 - Expander most expensive by far (25-50% eqp't)
 - Axial turbo (>5MW)
 - Radial turbo (200kW – 5MW)
 - Twin Screw (50kW – 500kW)
 - Efficiency (65% - 85%), “right to the bottom line”
- Heat Exchangers
 - Evaporator, preheater, condenser
 - Shell/tube for >~500kW, Plate/fin for <~200kW
- Pump
- BOP (valves, receivers, instruments, etc.)

Focus on Expander



Installed Cost

- Cap cost, \$/kW $\sim f(\text{kW}, \text{ORC temp})$
- Installation $\sim 50\text{-}100\%$ equipment cost
 - Site specific: height above grade, dist between source and ORC, etc.
 - Modular vs. 'stick built'
 - Air vs. water cooled



In Conclusion.....

□ Rules of Thumb

- Liquid sources below 190F and gas below 400F are too cold
- Sources below 5 MM Btu/h are too small
- Stay away from dirty and/or corrosive gases
- ORC beats steam below 700F and 10MW_e
- ORC needs base load source; 7000 h/y
- Don't get too excited about efficiency. Focus on \$/kW and uptime
- After selecting the ORC refrigerant the most important item is the expander

